AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Currently amended) A method of producing low-temperature coke, in which granular coke is heated to a temperature of 700 to 1050°C in a fluidized-bed reactor by an oxygen-containing gas, comprising introducing from below a first gas or gas mixture through at least one gas supply tube into a mixing chamber of the fluidized-bed reactor, the at least one gas supply tube being at least partly surrounded by a stationary annular fluidized bed which is fluidized by supplying fluidizing gas, and adjusting gas velocities of the first gas or gas mixture and ~~of~~ the fluidizing gas for the stationary annular fluidized bed ~~wherein the gas velocities have a~~ such that the Particle-Froude-Number is a) in the at least one gas supply tube between 1 and 100, b) in the stationary annular fluidized bed between 0.02 and 2, and c) in the mixing chamber between 0.3 and 30.

2. (Previously presented) The method as claimed in claim 1, wherein the Particle-Froude-Number in the at least one gas supply tube is between 1.15 and 20.

3. (Previously presented) The method as claimed in claim 1 wherein the Particle-Froude-Number in the stationary annular fluidized bed is between 0.115 and 1.15.

4. (Previously presented) The method as claimed in claim 1, wherein the Particle-Froude-Number in the mixing chamber is between 0.37 and 3.7.

5. (Previously presented) The method as claimed in claim 1, wherein solids are discharged from the fluidized-bed reactor and separated in a separator, wherein part of the solids or an amount of a product stream are recirculated to the stationary annular fluidized bed.

6. (Previously presented) The method as claimed in claim 5, wherein the amount of the product stream recirculated to the stationary annular fluidized bed is controlled by a difference in pressure above the mixing chamber.

7. (Currently amended) The method as claimed in claim 1, wherein ~~the~~ granular coal having a grain size of less than 10 mm is supplied to the fluidized-bed reactor as a starting material.

8. (Currently amended) The method as claimed in claim 1, wherein ~~the~~ granular coal is a highly volatile coal and the highly volatile coal is supplied to the fluidized-bed reactor as starting material.

9. (Previously presented) The method as claimed in claim 1, wherein the fluidizing gas supplied to the fluidized-bed reactor is air.

10. (Currently amended) The method as claimed in claim 1, wherein the pressure in the fluidized-bed reactor is between 0.8 and 10 bar.

11. (Previously presented) The method as claimed in claim 1, wherein iron ore is additionally supplied to the fluidized-bed reactor.

12. (Previously presented) The method as claimed in claim 11, wherein the iron ore is preheated before being supplied to the fluidized-bed reactor.

13. (Currently amended) The method as claimed in claim 11 [[10]], wherein a product of iron ore and low-temperature coke is withdrawn from the fluidized-bed reactor, wherein the product has a weight ratio of iron to carbon of 1:1 to 2:1.

14. (Currently amended) A plant for producing low-temperature coke, by the method as claimed in claim 1, comprising a fluidized-bed reactor, wherein the fluidized-bed reactor comprises at least one ~~has a~~ gas supply ~~system~~ tube at least partially surrounded by an annular chamber in which a stationary annular fluidized bed is located, and a mixing chamber being located above the upper orifice of the at least one gas supply tube, wherein the ~~which is formed such that~~ gas flowing through the at least one gas supply ~~system~~ tube entrains solids from [[a]] the stationary annular fluidized bed~~, which at least partly surrounds the gas supply system,~~ into the mixing chamber when passing through the upper orifice region of the at least one gas supply tube.

15. (Currently amended) The plant as claimed in claim 14, wherein the ~~gas supply system has~~ at least one gas supply tube ~~which~~ in the lower region of the fluidized-bed reactor extends upwards substantially vertically into the mixing chamber of the fluidized-bed reactor~~, the at least one gas supply tube being surrounded by a chamber which at least partly annularly extends around the at least one gas supply tube and in which the stationary annular fluidized bed is formed~~.

16. (Previously presented) The plant as claimed in claim 15, wherein the at least one gas supply tube is arranged approximately centrally with reference to the cross-sectional area of the fluidized-bed reactor.

17. (Previously presented) The plant as claimed in claim 14, wherein downstream of the fluidized-bed reactor there is provided a separator for separating solids, which has a solids return conduit leading to the annular fluidized bed of the fluidized-bed reactor.

18. (Currently amended) The plant as claimed in claim 14, wherein in the annular chamber of the fluidized-bed reactor, a gas distributor is provided, which divides the annular chamber into an upper fluidized bed region and a lower gas distributor chamber, and ~~that~~ wherein the gas distributor chamber is connected with a supply conduit for fluidizing gas.

19. (Previously presented) The plant as claimed in claim 14, wherein upstream of the fluidized-bed reactor, a preheating stage is provided, which consists of a heat exchanger and a separator.

20. (New) The method as claimed in claim 1, wherein the gas flowing through the at least one gas supply tube entrains solids from the stationary annular fluidized bed into the mixing chamber when passing through the upper orifice region of the at least one gas supply tube.